

**ETHYL ALCOHOL FROM MOLASSES
PLANT DESIGN
WITH CAPACITY 40,000 TON/YEAR**



By:
Ambar Tri Wahyuni
D500102001

Supervisors:

- 1. Rois Fatoni, ST, MSc, Ph.D**
- 2. Dr. Ir. Ahmad M. Fuadi**

**CHEMICAL ENGINEERING DEPARTMENT
FACULTY OF ENGINEERING
UNIVERSITAS MUHAMMADIYAH SURAKARTA
2017**

FACULTY OF ENGINEERING
UNIVERSITAS MUHAMMADIYAH SURAKARTA

Student's Name : Ambar Tri Wahyuni
Student ID# : D500102001
Design Project Title : Ethyl Alcohol From Molasses Plant Design With Capacity 40,000 Ton/Year
Supervisors : 1. Rois Fatoni, ST, MSc, Ph.D
 2. Dr. Ir. Ahmad M. Fuadi

Surakarta, April 27, 2017

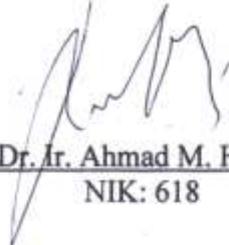
Approved by:

Supervisor #1



Rois Fatoni, ST, MSc, Ph.D
NIK: 892

Supervisor #2



Dr. Ir. Ahmad M. Fuadi
NIK: 618

Dean of Engineering Faculty



Ir. Sri Sunarjono, M.T., PhD
NIK: 682

Head of Chemical Engineering Department



Rois Fatoni, ST, MSc, Ph.D
NIK: 892

Author's Declaration

I, the undersigned below:

Student's Name : Ambar Tri Wahyuni
Student ID# : D500122008
Study Program : Chemical Engineering (International program)
Design Project Title : Ethyl Alcohol From Molasses Plant Design With Capacity 40,000 Ton/Year

Hereby declare that I am the sole author of this project report, except the quotes, data, summaries, and other materials which I clearly cite their references.

I understand that if it is proven otherwise, my degree may be confiscated.

Surakarta, April 27 2017



Ambar Tri Wahyuni

ABSTRACT

Ethyl alcohol is the principal type of alcohol in alcoholic beverages. Ethyl alcohol is mostly produced by the fermentation of sugar by yeast or by petrochemical processes. Ethyl alcohol is a chemical product primarily used for antiseptic, antidote, medical solvent, recreational, fuel (engine fuel, rocket fuel, fuel cells), household heating, feedstock, solvent, and low temperature liquid(used in laboratories with dry ice or other coolants). The plant of ethyl alcohol from molasses as raw material will be established in Sukoharjo, Central Java with capacity 40,000 tons/year and built in year 2020. The raw of molasses is obtained from some suppliers around Solo – Semarang, Central Java. The production of ethyl alcohol is carried out in a fermenter where the operating condition of pressure and temperature are 1 atm and isothermally at 35°C, respectively. Utility needs to support the process. Used water as much as 187,154.6378 kg/h which is obtained from river water. Air and compressed air as much as 50 m³/h also needs to suport the process. The other utilities needs is steam 66,767,052.8459 kg/h and electricity 350 kw/h.

This ethyl alcohol plant has 330 operational days with Fixed Capital as much as Rp 74,261,326,185.2297 and known the Working Capital as much as Rp 45,472,670,854.7867. From the economic evaluation that had been calculated before showed that the Profit before tax is about Rp 25,002,027,285.4679, while the Profit after tax about Rp 17,501,419,099.8275. From the calculation also known that the Return On Investment before tax is about 33.6676%, while Return On Investment after tax is about 23.5673%. The Pay Out Time before tax shown the number of 2.2900 years with Pay Out Time after tax are 2.9791 years. Break Event Point is 53.8313% and Shut Down Point is about 41.2793%, and Discounted Cash Flow as much as 30.2125%. From the results of economic evaluation this Ethyl alcohol plant is feasibly established and operated.

FOREWORD



Assalamu'alaikum Wr. Wb.

Alhamdulillah, all praises be to Allah SWT who has given many mercies and blessing so the author can finish the Final Project of Chemical Plant Design without any troubles. Secondly, may peace be upon the prophet Muhammad SAW who has guided us from the darkness into the brightness.

Title for this Final Project is "Ethyl Alcohol From Molasses Plant Design With Capacity 40,000 Tons/Year". Every student in Chemical Engineering at Universitas Muhammadiyah Surakarta should take plant design as final project to be able to graduate as bachelor of engineering. With this final project, there is hope so analitical and teoritical while studying can be applied correctly.

This final asignment completion is supportted by many people around author, so in this opportunity, author would like to express the sincere thanks to all who helped resolve this research report, especially to :

1. Mr. Rois Fatoni, S.T, M.Sc, PhD as Chemical Engineering Department Chief and author 1st supervisor.
2. Mrs. Eni Budiati, S.T., M.Eng as final project coordinator.
3. Mr. Dr. Ahmad M. Fuadi as author 2nd supervisor.
4. Ir. Herry Purnama, Ph.D and Ir. Haryanto AR, M.S as evaluator of this final project.
5. Author parents that always give a lot of love, pray, and support at home. So author can finish this final project.
6. Author husband Nurohman Sigit H, who have help in process writing and give some spirit when author get down also give a lot of love so the author can done this final asignment.
7. All lecturers at Muhammadiyah University of Surakarta.
8. All family that always prays and support author.
9. All help from friends in Muhammadiyah University of Surakarta.

Author is aware this final assignment still have a lot of flaws and it's far from perfection. Author expects hopefully this report can be useful for those who need information about the material covered in this report.

Wassalamu'alaikum Wr. Wb.

Surakarta, April 2017

Author

CONTENT

TITLE PAGE	i
APPROVAL PAGE	ii
AUTHOR DECLARATION.....	iii
ABSTRACT	iv
FOREWORD	v
CONTENT	vii
FIGURE CONTENT	x
GRAPH CONTENT	x
TABLE CONTENT	xi
BAB. I INTRODUCTION	1
1.1. Background	1
1.2. The Selection of Design Capacity	6
1.3. The Selection of Plant Location	8
1.4. Theory	10
1.4.1 Type of Process	10
1.4.2 Product Usability	12
1.4.3 General Theory	12
BAB. II PROCESS DESCRIPTION	14
2.1. Raw Material and Product Specification	14
2.1.1. Raw Material Specification.....	14
2.1.2. Product Specification.....	17
2.1.3. Adjuvant Specification.....	18
2.2. Reaction Concept	21
2.2.1. Basic Reaction	21
2.2.2. Reaction Characterity	21
2.2.3. Reaction Phase	23
2.2.4. Operating Condition	23
2.3. The Step of The Process	24
2.3.1. Molasses Process	24

2.3.2. Molasses Sterilization	24
2.3.3. Yeast Culturization	24
2.3.4. Fermentation	25
2.3.5. Filtering	25
2.3.6. Purification Process.....	26
2.4. Mass Balance And Heat Balance	27
2.4.1. Mass Balance	27
2.4.2. Heat Balance	40
2.5. Plant Layout And Equipment.....	54
2.5.1. Plant Layout	54
2.5.2. Equipment Placement	58
BAB. III PROCESS EQUIPMENT	60
BAB. IV UTILITY AND LABORATORY UNITS	88
4.1. Utility	88
4.1.1. Water Processing and Supply Units.....	89
4.1.2. Steam Generator Unit.....	96
4.1.3. Compressed Air Supply Unit.....	97
4.1.4. Power Generator Unit.....	97
4.1.5. Fuel Supply Unit.....	100
4.1.6. Waste Processing Unit...	101
4.2. Laboratory	101
BAB. V COORPERATE MANAGEMENT	109
5.1. Coorporate Form	109
5.2. Organization Structure	110
5.3. Task and Authority.....	113
5.3.1. Shareholder.....	113
5.3.2. Commisioner Board.....	113
5.3.3. Director Board.....	113
5.3.4. Expertise Staff.....	114
5.3.5. Manager.....	114
5.3.6. Head Division.....	116

5.3.7. Section Head.....	116
5.4. Employee Work Hour	116
5.4.1. Non-Shift Employee.....	116
5.4.2. Shift Employee.....	117
5.5. Position Classification, Staff Number, and Salary	118
5.5.1. Position Requirement.....	118
5.5.2. Staff Number and Salary Break Down.....	119
5.6. Employee Prosperity.....	120
5.7. Production Management.....	120
5.7.1. Production Planning.....	121
5.7.2. Production Control.....	122
BAB. VI ECONOMIC EVALUATION	123
6.1. Capital, Manufacturing Cost, General Expanses, and Financial Analysis	123
6.1.1. Total Fixed Capital Investment.....	126
6.1.2. Working Capital.....	127
6.1.3 Manufacturing Cost.....	127
6.1.4. General Expense	128
6.1.5. Economic Evaluation Calculation	128
6.1.6. Apropriateness Analysis.....	128
BAB. VII CONCLUSION.....	133
REFERENCE	
ATTACHMENT	

Figure Content

Figure 1.1. Fossil Fuel Consumption in Indonesia (in KL)	1
Figure 1.2. Comparation of crude oil need from import and local(mil barrel)	3
Figure 1.3. Fossil fuel consumption in 2011	4
Figure. 1.4. Production of Ethyl Alcohol	11
Figure 2.1. Qualitative Flow Diagram	38
Figure 2.2. Quantitative Flow Diagram	39
Figure 2.3. Plant placement.....	57
Figure 2.4. Plant layout	59
Figure 3.1. Inoculation Tank Scheduling	44
Figure 3.2. Fermentor Reactor Scheduling	46
Figure 4.1. River Water Process as a Support Process	101
Figure 5.1. Coopperate Structure	109
Figure 6.1. Equation Graph Cost Index with Year.....	121
Figure 6.2. Economic Evaluation	129

Table Content

Table 1.1. Government Expanding and Subsidy in Quintillion of Rupiah	5
Table 1.2. Ethanol (Ethyl Alcohol) Product Data	7
Table 1.3. Data of Ethyl Alcohol plant	8
Table 2.1 Molasses composition	14
Table 2.2 Mass balance around dilute tank M – 01.....	27
Table 2.3 Mass balance around sterilization tank F – 101	27
Table 2.4. Mass balance around storage tank F – 102.....	28
Table 2.5. Inoculation tank R – 01 mass balance.....	29
Table 2.6. Reactor R – 02 mass balance	30
Table 2.7. Mass balance around filter H – 01.	31
Table 2.8. Mass balance around separator D – 01.....	32
Table 2.9. Mass balance around 1 st distillation column D – 02	33
Table 2.10. Mass balance around 2 nd distillation column D – 03.....	34
Table 2.11.Overall mass balance	35
Table 2.12.Overall mass balance (cont.)	36
Table 2.13. Heat balance around dilute tank M – 01	40
Table 2.14. Heat balance around sterilization tank F – 101	40
Table 2.15. Heat balance around culturization tank R – 01	41
Table 2.16. Heat balance around reactor R – 02	42
Table 2.17. Heat balance around filter H – 01	43
Table 2.18. Heat balance around separator D – 01	44
Table 2.19. Heat balance around 1 st distillation column D – 02	45
Table 2.20. Heat balance around 2 nd distillation column D – 03	46
Table 2.21. Heat balance around cooler E-100.....	46
Table 2.22. Heat balance around heater E-200.....	47
Table 2.23. Heeat balance around cooler E – 103	48
Table 2.24. Heat balance around cooler E – 101.....	49
Table 2.25. Heat balance around cooler E – 104.....	50
Table 2.26. Heat balance around cooler E – 105.....	51

Table 2.27. Heat balance around cooler E – 106.....	51
Table 2.28. Overall heat balance.....	52
Table 2.29. Overall heat balance (Cont.).....	53
Table 2.30. Wide of plant area.....	56
Table 3.1. Molasses storage tank F – 100 specification.....	60
Table 3.2. Molasses storage tank F – 100 specification (Cont.).....	61
Table 3.3. Sterilization tank F – 101 specification	61
Table 3.4. Sterilization tank F – 101 specification (Cont.)	62
Table 3.5 Temporary storage tank F – 102 specification.....	62
Table 3.6. Storage tank F – 103 specification.....	63
Table 3.7. Dilute tank M – 01 specification.....	64
Table 3.8. Cooler E – 100 specification.....	65
Table 3.9. Cooler E – 101 specification.....	66
Table 3.10. Cooler E – 103 Specification	67
Table 3.11. Cooler E – 104 specification	68
Table 3.12. Cooler E – 105 specification	69
Table 3.13. Cooler E – 106 specification	70
Table 3.14. Heater E – 200 specification	71
Table 3.15. Blower G – 01 specification.....	72
Table 3.16. Inoculation tank R – 01 specification	72
Table 3.17. Inoculation tank R – 01 specification (Cont.).....	73
Table 3.18. Reactor R – 02 specification	75
Table 3.19. Rotary drum filter H – 01 specification	77
Table 3.20. Separator D – 01 specification	77
Table 3.21. 1 st Distilation column D – 02 specification.....	78
Table 3.22. Condensor E – 301 specification	79
Table 3.23. Accumulator F – 201 specification	80
Table 3.24. Reboiler E – 401 specification	80
Table 3.25. Reboiler E – 401 specification (Cont.).....	81
Table 3.26. 2 nd distilation column D – 03 specification.....	82
Table 3.27. Condensor E – 302 specification	83

Table 3.28. Accumulator F – 202 specification	84
Table 3.29. Reboiler E – 402 specification	84
Table 3.30. Reboiler E – 402 specification (Cont.).....	85
Table 3.31. Main pump equipment specification.....	86
Table 3.32. Main pump equipment specification (Cont.)	87
Table 4.41. Water needs.....	91
Table 4.2. Water needs (Cont.)	92
Table 4.3. Steam needs in plant	96
Table 4.4. Process power data	98
Table 4.5. Utility power needs	99
Table 4.6. Other electricity needs.....	100
Table 4.7. Main utility equipment specification.....	105
Table 4.8. Main utility equipment specification (Cont.).....	106
Table 4.9. Utility pump specification.....	107
Table 4.10. Utility pump specification (Cont.).....	108
Table 5.1. Shift employee work hour	117
Tabel.5.2. list of position and requirement.....	118
Tabel.5.3. Brake down position, staff number and salary.....	119
Table 6.1. Chemical plant cost index.....	124
Table 6.2. Total fixed capital investment.....	126
Table 6.3. Working capital investment	127
Table 6.4. Manufacturing cost	127
Table 6.5. General expenses	128
Table 6.6. Fixed cost	130
Table 6.7. Variable cost	130
Table 6.8. Regulated Cost	130
Table 7.1. Economic feasibility analysis	133

MOTTO

- ✓ **If you can dream you can do it**
- ✓ **Do the best, be good, then you will be the best**
- ✓ **Keep thinking the out of the box, keep executing the inside of the box**

Presented

- ❖ All praises be to Allah SWT who has given many mercies and blessing so the author can finish the Final Asignment of Chemical Plant Design without any troubles.
- ❖ May peace be upon the prophet Muhammad SAW who has guided us from the darkness into the brightness.
- ❖ Mom and Dad, thanks for the love, pray, and support so I can be like this. Thanks for all that you have given to me. I just can say thank you and I love you all.
- ❖ My lovely hubby, thank you so much for all that you have given to me, I love you so much.
- ❖ All family that give me support until now.

Hopefully what I studied before can helps others. Aamiin.